

Linear R-T.

and

ICF Background

Lect. 3-4-5

Rayleigh - Taylor Instability \leftrightarrow A Case Study

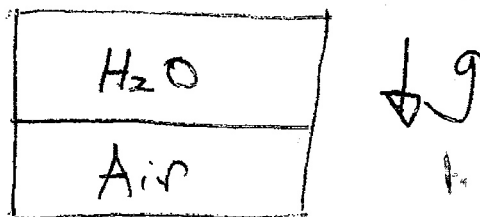
2.) Motivation and ICF Overview

- \rightarrow RT is simple example/paradigm of non-trivial nonlinear collective dynamics
- \rightarrow intellectual content typical of current problems in plasma physics

\rightarrow nonlinear evolution of instabilities
turbulence, transport, etc.

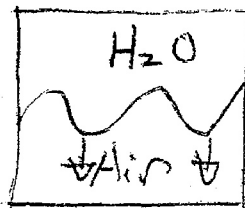
Overview of RT Physics:

I) Consider:



- free energy available (i.e. gravitational potential energy) (free energy \leftrightarrow instability) (successful storage \leftrightarrow confinement)
- system in equilibrium (i.e. inverted glass H_2O + cardboard) but small interface perturbations grow.

i.e.



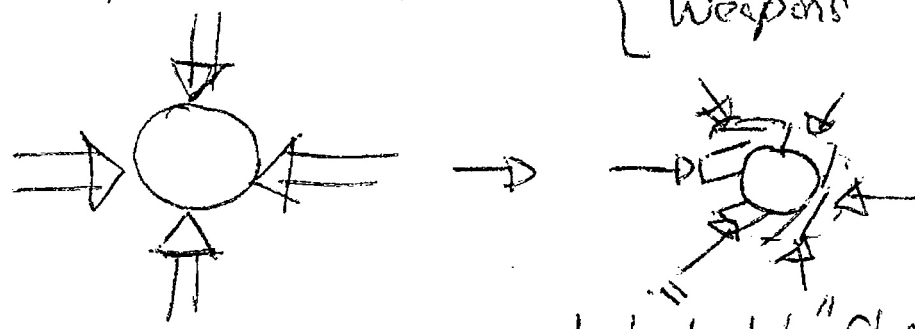
water-glass demo.

II) - typical evolutionary history:

→ instability occurs when light fluid accelerated into heavy fluid

⇔ in light fluid frame equivalent to inverted water glass

Imp: Importance R-T in ICF $\frac{\rho_1}{\rho_2} \frac{v_1}{v_2}$
 e.g. spherical implosions } Weapons etc.



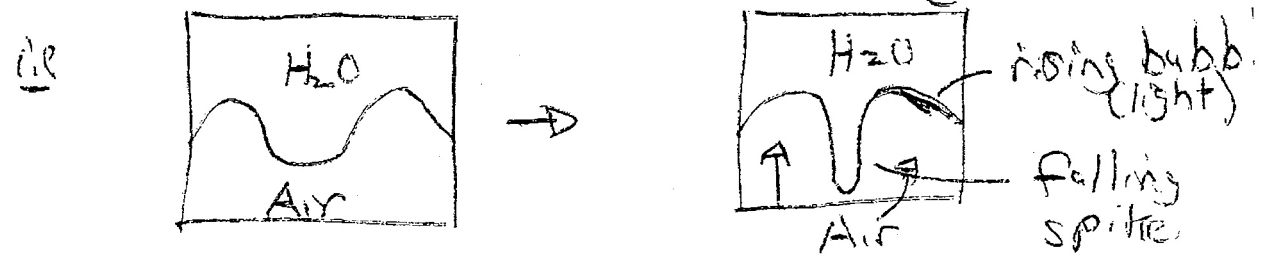
hot "light" fluid accelerated into "heavy" core
 ablation-drives rocket

① → $\epsilon < \lambda \rightarrow$ linear growth phase

i.e. $\vec{\epsilon}_k = \vec{\epsilon}(0) e^{\gamma t}$

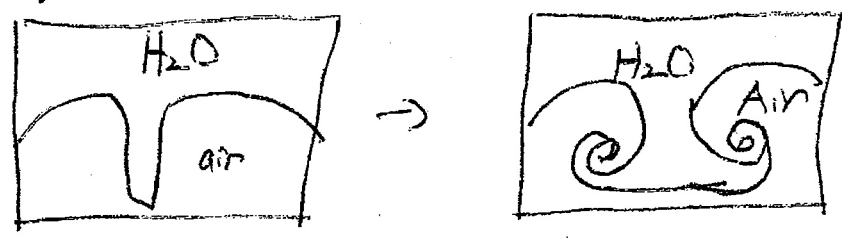
↳ calculated from linear perturbation analysis

② → $\epsilon \gtrsim \lambda \rightarrow$ Spikes and Bubble } Formation Competition



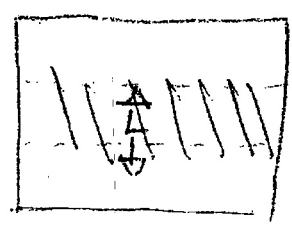
③ $\epsilon \gtrsim \lambda \rightarrow$ Secondary Instability / Bubble Competition

- Spike undergoes Kelvin-Helmholtz (shearing) instability
- spike "rolls up" and is "blunted"



④ $\epsilon \gg \lambda \rightarrow$ Turbulent Mix

- spike undergoes KH \rightarrow turbulence generated
- spike + bubble ensemble \Rightarrow mixing layer, growing in time



phenomenological
 \downarrow

$$L \sim (0.05) \frac{(\rho_w - \rho_a) g t^2}{(\rho_w + \rho_a)}$$

intuition from elementary mech.

Note:

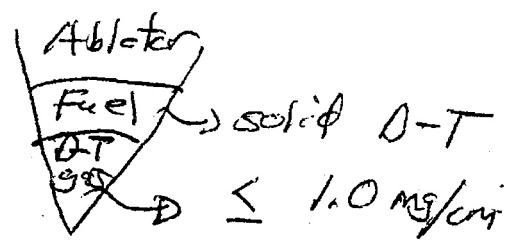
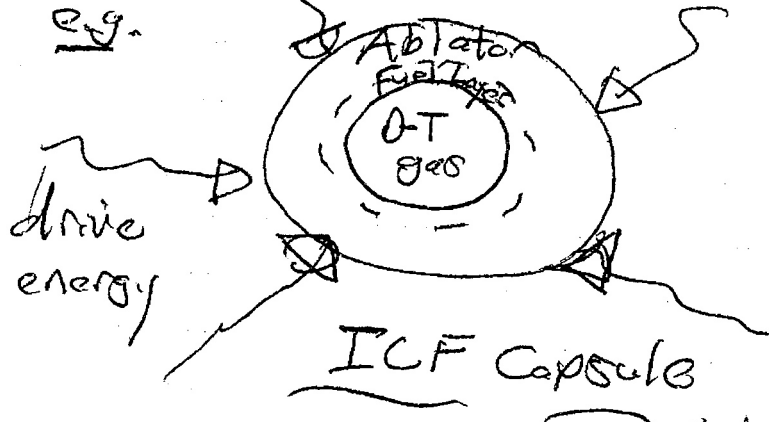
- (i) Representation
- ① \rightarrow Fourier Modes
 - ②, ③ \rightarrow Structures (Spike, Bubble)
 - ④ \rightarrow Turbulence

→ R-T in ICF

a.) Some Basics of ICF

ICF: I for Inertial

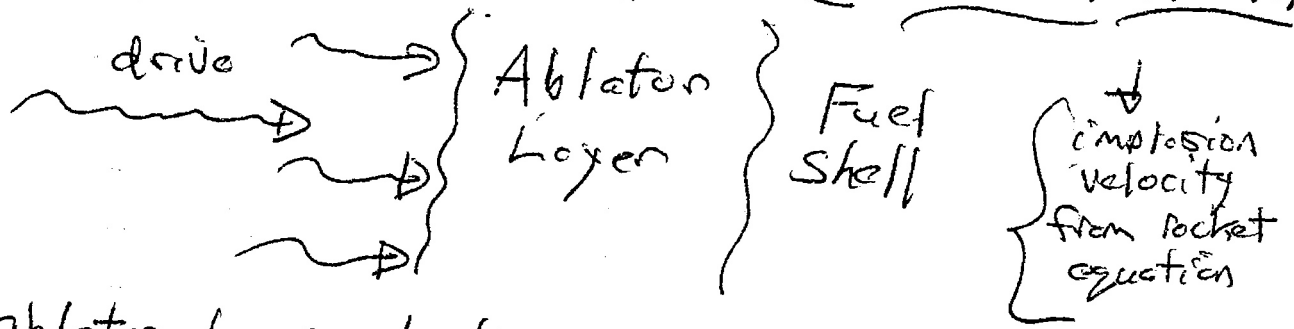
eg.



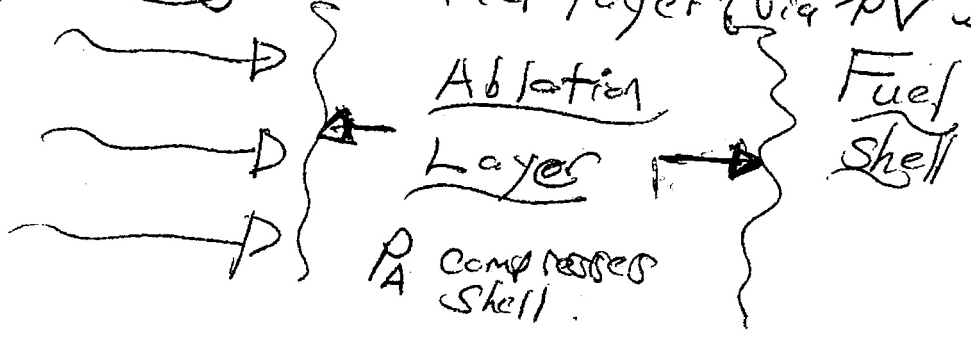
"drive" = laser or x-rays

How it works:

Ablation-Driven Rocket



ablator layer heats and expands thus compressing inner fuel layer (via PV work)



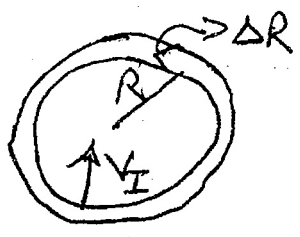
note: → "implosion" is just conservation of momentum between expanding ablator layer and inner shell

→ W_{OF} (work on fuel) $\sim P_A V_{st}$

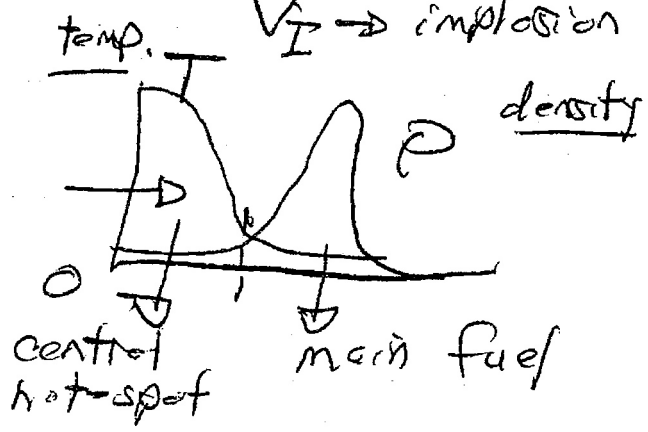
\downarrow ablation pressure
 \downarrow V_{shell}

∴ for fixed P_A (determined by driver and materials), larger, thin shells can be accelerated better than small thick ones.

→ expected (hoped for...) final state seq:

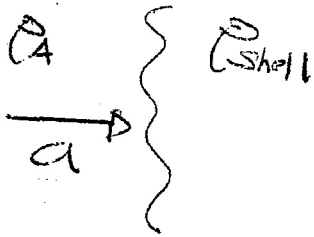


R → shell radius
 ΔR → shell thickness
 V_I → implosion velocity



idea is that burn initiates in central hot-spot, then propagates to main fuel shell.

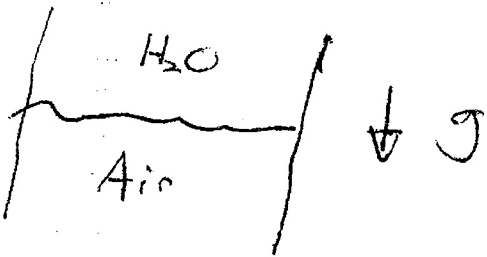
Now! Consider situation:



$$P_{shell} > P_A$$

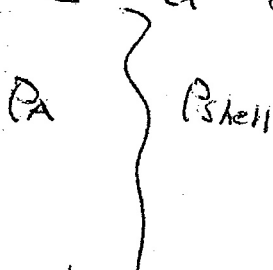
i.e. Light fluid "pushing on" (i.e. accelerating into) heavy fluid

Compare to inverted glass of H_2O :



$$P_{H_2O} > P_{air}$$

i.e. in frame of ablator, above interface:



\Rightarrow Rayleigh Taylor Instability!

\Rightarrow PGS. 1-2

Important features of Implosion :

→ IFAR - in flight aspect ratio
(→ stability)

$$IFAR = \frac{R}{\Delta R}(t)$$

$\Delta R < \Delta R(t=0)$
due compr.

→ seek large IFAR

→ but R-T_i constrains upper limit
on IFAR → broadens ΔR via mixing

i.e. $25 < IFAR < 135$

⇒ sets minimum P_A (~ 100 Mbar)
and irradiance absorbed ($\sim 10^{15}$ W/cm²)
for MJ drivers in order to achieve
 $v_I \sim 3-4 \times 10^7$ cm/sec.

⇒ R-T_i is (partly) why NIF costs
> 1 BB i.e. drives cost of laser.

→ C_n - convergence ratio
(→ symmetry)

$$C_n = R_{a,i} / r_{hot spot, f}$$

$i \rightarrow$ initial
 $f \rightarrow$ final

ie deviation from sphericity can destroy hot-spot (burn-through) etc,

$$\delta R = \frac{1}{2} dg t^2 = \frac{dg}{g} (R_A - r) = \frac{dg}{g} R (C_n - 1)$$

\downarrow deviation from sphericity \downarrow deviation from avg. acceleration

Tolerable asymmetry \Rightarrow excess of k.E. above ignition threshold. If demand, say

$$\delta R < \frac{R}{4} \Rightarrow \frac{dg}{g} \sim \frac{dV}{V} < \frac{1}{4(C_n - 1)}$$

since $C_n < 40$, need $\frac{dV}{V} \lesssim 1\% !!$

\rightarrow $\left\{ \begin{array}{l} \text{Point is that R.T. } \Rightarrow \text{ ripples } \Rightarrow \text{ asymmetry} \\ \text{Can destroy implosion via } \bullet \text{ inducing} \\ \text{asymmetry } \bullet, \text{ unless } kE \gg \text{ ignition threshold} \end{array} \right.$

\downarrow
Laser drive

once again, R.T. \Rightarrow ~~§~~

(ii) Evolution : ① \rightarrow exponential

②, ③ \rightarrow transition to algebraic

④ \rightarrow algebraic

Step, in favor II.
 III) Application II here
 = ICF

Controlled Fusion $\Leftrightarrow n T T > (n T T)_{\text{Lawson}}$

Confinement \rightarrow magnetic (tokamaks, etc.)

\rightarrow inertial (Laser acceleration, gravity (star))

\rightarrow ICF :

\rightarrow confine burning plasma via implosion driven by laser-produced ablation

\rightarrow implosion drives $n T T > (n T T)_{\text{Lawson}}$

Further :

\rightarrow optimal to implode shell :



acceleration \rightarrow outer surface
 (laser pulse) \rightarrow ablated
 \rightarrow RT unstable

deceleration \rightarrow inner mass
 (post pulse) \rightarrow accelerated into
 inner shell
 \rightarrow RT unstable

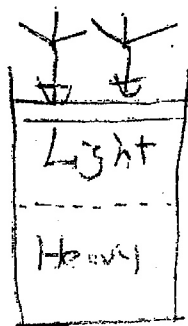
→ implosion instability is intrinsic to ICF

∴ Need understand, minimize

→ Basic Insight

- Computer Simulations
- Laboratory Experiments

Experimental Set-Up (Youngs Rocket Rig, D. Youngs, AWE)



→ Rocket Engine:

- Easy:
 - diagnosis
 - flow visualizations

References:

Landau, Lifshitz; Fluid Mechanics (Linear Theory)

D. H. Sharp, Physica 120 (1984) B.3 (overview)

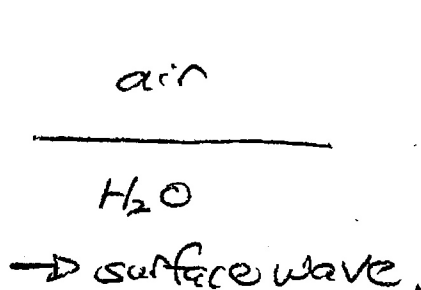
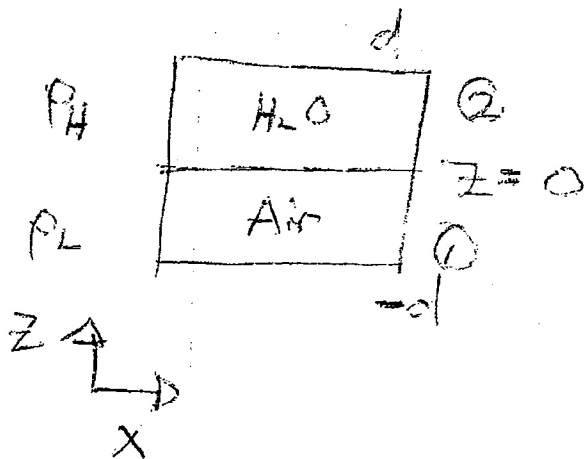
S. Chandrasekhar "Hydrodynamic and Hydromagnetic Stability" Oxford U. Press (Linear Theory)

H. J. Kull, Physics Reports 206 #5 1991 (Review)

→ water face 6.
 → finite thickness

b.) Linear Theory

I) Hydrodynamic RT / Plane Slab



Now, consider:

- incompressible fluid (i.e. $\gamma \ll kc$)

$$\nabla \cdot \underline{v} = 0$$

- irrotational flow $\nabla \times \underline{v} = \underline{\omega} = 0$
 (piecewise uniform density)

III → Newton's tube

$$\nabla \times \underline{v} = 0 \Rightarrow \underline{v} = \nabla \phi$$

Stream Function

$$\nabla \cdot \underline{v} = 0$$

$\Rightarrow \nabla^2 \phi = 0 \Leftrightarrow$ R.T. instability is potential flow problem

z

Now, $\phi = \sum_H \phi_H(z) e^{ikx}$ (∞ -ly wide or periodic box)

$\frac{\partial^2 \phi_H(z)}{\partial z^2} - k^2 \phi_H = 0 \Rightarrow$ origin of $\left\{ \begin{array}{l} \rho \\ \phi \end{array} \right.$ continuity

For $kd \gg 1$, neglect finite depth, so

$\phi_H = \begin{cases} \phi_H^{(1)} e^{kz} & z < 0 \quad (1) \\ \phi_H^{(2)} e^{-kz} & z > 0 \quad (2) \end{cases}$

(satisfy $v_n = 0$)
bdry

At $z=0$:

$\rho^{(1)} = \rho^{(2)} \rightarrow$ pressure continuity

(else interface motion on acoustic time scale)

$\left. \frac{\partial \phi^{(1)}}{\partial z} \right|_0 = \left. \frac{\partial \phi^{(2)}}{\partial z} \right|_0 \rightarrow$ normal velocity continuity

For dynamics:

\rightarrow described entirely by interface motion

i.e. 

\rightarrow fields: $\eta(x, z, t) \rightarrow$ instantaneous interface position

$\phi(x, z, t) \rightarrow$ stream fun

\downarrow
 $z = 0 \mp \eta$

\swarrow why NLT hard.
(η dropped for linearized theory)

or stream function:

(Bernoulli's law)

$$\rho \left(\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \nabla \underline{v} \right) = -\nabla p - \rho g \quad (g = -g \hat{z})$$

$$\underline{v} = \nabla \phi$$

$$\rho \left(\frac{\partial}{\partial t} \nabla \phi + \nabla \phi \cdot \nabla \nabla \phi \right) = -\nabla p - \rho g$$

$$\rho \left(\frac{\partial}{\partial t} \nabla \phi + \nabla \left(\frac{\nabla \phi \cdot \nabla \phi}{2} \right) \right) = -\nabla p - \rho g$$

$$\Rightarrow \boxed{\frac{\partial \phi}{\partial t} + \frac{\nabla \phi \cdot \nabla \phi}{2} = -\frac{p}{\rho} - g \eta} \quad (\underline{v} = \nabla \phi)$$

i.e. $\frac{\partial \phi}{\partial t} = 0 \Rightarrow \rho + \frac{\rho v^2}{2} = \text{const.}$
 $g = 0$

For interface:

$$\boxed{\frac{\partial \eta}{\partial t} + \nabla \phi \cdot \nabla \eta = \frac{d\eta}{dt} = \frac{\partial \phi}{\partial z}} \rightarrow \text{definition}$$

Then, linearizing for R.I. mode:

$$\frac{\partial \tilde{\phi}}{\partial t} = -\frac{\tilde{p}}{\rho} - g \tilde{\eta}$$

$$\frac{\partial \tilde{\eta}}{\partial t} = \frac{\partial \tilde{\phi}}{\partial z}$$

thus:

$$\rho_2 \frac{\partial \tilde{\phi}^{(2)}}{\partial t} + g \rho_2 \tilde{\eta} = -\tilde{\rho}^{(2)} \quad (e^{-kz})$$

$$\rho_1 \frac{\partial \tilde{\phi}^{(1)}}{\partial t} + g \rho_1 \tilde{\eta} = -\tilde{\rho}^{(1)} \quad (e^{kz})$$

At interface: $\tilde{\rho}^{(1)}|_0 = \tilde{\rho}^{(2)}|_0$

$$\rho_2 \frac{\partial \tilde{\phi}^{(2)}}{\partial t} + g \rho_2 \tilde{\eta} = \rho_1 \frac{\partial \tilde{\phi}^{(1)}}{\partial t} + g \rho_1 \tilde{\eta}$$

$$\tilde{V}_z^{(1)}|_0 = \tilde{V}_z^{(2)}|_0$$

$$\Rightarrow +k \tilde{\phi}^{(1)} = -k \tilde{\phi}^{(2)}$$

\Rightarrow

$$g(\rho_2 - \rho_1) \tilde{\eta} = \rho_1 \frac{\partial \tilde{\phi}^{(1)}}{\partial t} - \rho_2 \frac{\partial \tilde{\phi}^{(2)}}{\partial t}$$

$$= (\rho_1 + \rho_2) \frac{\partial \tilde{\phi}^{(1)}}{\partial t}$$

$$\therefore \frac{\partial \tilde{\phi}^{(1)}}{\partial t} = g \frac{(\rho_2 - \rho_1)}{(\rho_1 + \rho_2)} \tilde{\eta}$$

$$\frac{\partial \tilde{\eta}}{\partial t} = \frac{\partial \tilde{\phi}^{(1)}}{\partial z}$$

t.

$$\frac{\partial^2 \tilde{\phi}^{(v)}}{\partial z^2} = g \frac{(\rho_2 - \rho_1)}{(\rho_2 + \rho_1)} \frac{\partial \tilde{\phi}^{(v)}}{\partial z}$$

$$\Rightarrow \omega_n^2 = -g A k$$

$$\boxed{\gamma = \sqrt{g A} \sqrt{k}}$$

$A \equiv \frac{\rho_2 - \rho_1}{\rho_2 + \rho_1}$
 Atwood # - available free energy

Comments:

(i) equivalent: { fluid with vacuum } $\rho \rightarrow A$

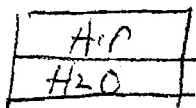
(ii) H₂O, air: $\lambda = 1 \text{ cm}$ $\gamma \sim 1 \text{ sec}^{-1}$
(fast)

(iii) $\gamma = \sqrt{g A k}$

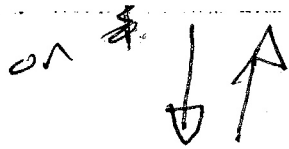
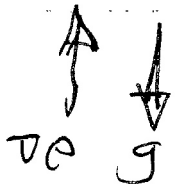
\therefore in absence of dissipation, surface tension etc., shorter wavelengths grow faster

(iv) $A < 0 \Rightarrow$ stable stratification
 \rightarrow surface buoyancy wave

H₂O, Air $\Rightarrow \omega = \sqrt{k g}$ \rightarrow surface gravity wave



light push on heavy



11.

- Other Effects:

(i.) Surface Tension (Fluid) \rightarrow III (HW)

- curvature of interface exerts force

i.e. $\rho \rightarrow \rho - \rho \gamma_T \nabla_n^2 \eta$ ($\gamma_T = \frac{T_s}{\rho}$)

(For H₂O - air, only H₂O feels surface tension; for fluid ①, fluid ②, T_s for each interface)

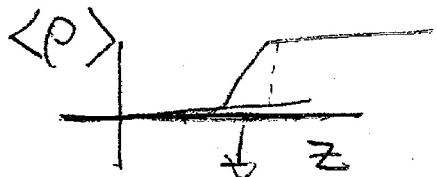
$\Rightarrow \gamma = (kgA - \gamma_T k^3)^{1/2}$

$k_{max} = (gA / \gamma_T)^{1/2}$
unstable

\rightarrow range of modes limited

eg. inverted glass with cardboard $\rightarrow \gamma_T \rightarrow \infty$
 \rightarrow high disp. of growth

(ii.) Finite Interface Thickness - $\nabla \rho$



finite layer thickness

Consider opposite limit:

$k L_p \gg 1$

$\bar{L}_p = \frac{1}{\rho} \frac{d\rho}{dz}$

rippled interface \rightarrow cell

- fluid motion not irrotational, as $\nabla \rho \neq \nabla p$
Hydrostatic eqn $\frac{dp}{dz} = -\rho g$

Review

→ Last time: $\nabla^2 \phi = 0$

$$\Rightarrow \begin{cases} \phi_H = \tilde{\phi}_H e^{-kz} \\ \phi_L = \tilde{\phi}_L e^{kz} \end{cases} \rightarrow \text{Bernoulli}$$

$$\left[\begin{array}{l} \rho_H \\ \rho_L \end{array} \right] \left\{ \begin{array}{l} \frac{\partial \phi}{\partial t} + \frac{(\nabla \phi)^2}{2} = -\frac{p}{\rho} + g\eta \\ \frac{\partial \eta}{\partial t} + \nabla \phi \cdot \nabla \eta = \frac{\partial \phi}{\partial z} \end{array} \right. \rightarrow \text{defn.}$$

$$\tilde{v}_{Hz} = \tilde{v}_{Lz} \quad \tilde{\rho}_H = \tilde{\rho}_L$$

LT. \Rightarrow

$$\gamma = \sqrt{gA k}$$

$$A = \left[\frac{\rho_H - \rho_L}{\rho_H + \rho_L} \right]$$

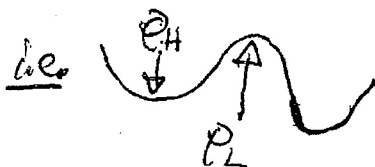
→ Key Assumptions:

- incompressible $\rightarrow \gamma \ll k c_s$
- inviscid $\rightarrow \gamma \gg \nu k^2$

- irrotational $\rightarrow \underline{v} = \nabla \phi$

- thin interface ("piecewise uniformity")
- no breaking \rightarrow amplitude restricted
- no k.H

$\Delta \rightarrow$ potential flow.



interface ripples

but "heavy" falls
"light" rises

then, for interface, natural to define :

$$dF_I = -S_I dT + \sigma dA,$$

↓
entropy
of interface

↳ change in free energy
due increase in surface
area of interface (treat as
separate phase)

$\sigma \equiv$ Surface Tension
E/area. ~~Work done per unit area~~

Hereafter, consider isothermal displacement.

$$\begin{aligned} \rightarrow dF &= -p_1 dV - p_2 (-dV) + \sigma dA \\ &= (p_2 - p_1) dV + \sigma dA \end{aligned}$$

interface expands 'into' 2nd material

Further: $dV = dA d\varepsilon$ (for surface)

↓ displacement
↑ $\varepsilon(x,y)$

For dA: $dA = \int dx dy \left(1 + \left(\frac{\partial \varepsilon}{\partial x} \right)^2 + \left(\frac{\partial \varepsilon}{\partial y} \right)^2 \right)^{1/2}$
- $\int dx dy$

∴ for small displacement:

$$dA \approx \int dx dy \left(1 + \frac{1}{2} \left(\frac{\partial \varepsilon}{\partial x} \right)^2 + \frac{1}{2} \left(\frac{\partial \varepsilon}{\partial y} \right)^2 \right)$$

$$dA = \int dx dy (-\nabla^2 \epsilon)^{1/2} d\epsilon$$

\downarrow
 curvature of
 surface displacement

(i.e. anticipates integration by parts)

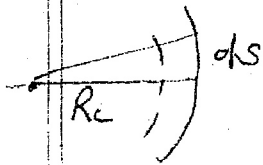
$$\frac{\delta}{\delta \epsilon} dF = \int [(p_2 - p_1) dA_0 - \nabla^2 \epsilon dA_0] \delta \epsilon$$

\Rightarrow condition for equilibrium:

$$p_2 - p_1 = \nabla^2 \epsilon(x, y)$$

More generally: $dF = (p_2 - p_1) dA_0 d\epsilon + \nabla dA$

Now consider arbitrary (i.e. not weakly curved interface)



$$\begin{aligned}
 ds' &= (R_c + d\epsilon) d\theta \\
 &= dl_0 \left(1 + \frac{d\epsilon}{R_c}\right)
 \end{aligned}$$

In general, surface parametrized by 2 radii of curvature R_1, R_2

$$\text{so } dA = \int dl_1 dl_2 \left(1 + \frac{d\epsilon}{R_1}\right) \left(1 + \frac{d\epsilon}{R_2}\right) = \int dl_1 dl_2$$

$$dA = \int h_1 dh_2 \left(\frac{1}{R_1} + \frac{1}{R_2} \right) d\epsilon$$

Thus, have most general expression:

$$dF = \int \left[(P_2 - P_1) dA_0 - \left(\frac{1}{R_1} + \frac{1}{R_2} \right) dA_0 \right] d\epsilon$$

thus, for equilibrium with interface:

$\gamma \left(\frac{1}{R_1} + \frac{1}{R_2} \right) = -(P_2 - P_1)$	Laplace's Law
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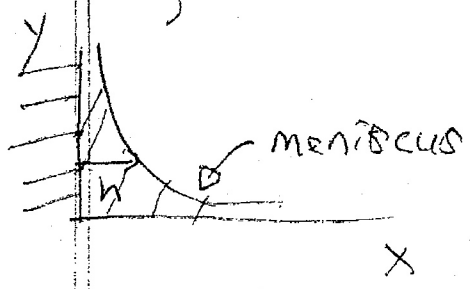
i.e. \rightarrow given 2-phase equilibrium (separated) can use to estimate droplet size for immiscible liquids

i.e. if $P_2 < P_1$

\therefore droplets of size $R \sim \gamma / (P_1 - P_2)$ may be expected.

\downarrow skip to IS

\rightarrow consider liquid adjacent to fixed vertical wall, then:



$h(y) \equiv$ defined thickness of meniscus

Then, can write:

$$p_{112} = p_0 - \rho g y(x) \quad \rightarrow \text{known} \quad (g < 0)$$

to calculate $h(y)$, use Laplace's Law:

ie.
$$p_0 - \rho g y = \frac{\sigma}{R_c}$$

but
$$\frac{1}{R_c} = \frac{-\partial^2 h / \partial x^2}{(1 + (\partial h / \partial x)^2)^{3/2}}$$

(ie. don't make small curvature approx)

then taking $p_0 = 0$ (ref):

$$+ \rho g y(x) = + \frac{\partial^2 h(y) / \partial x^2}{(1 + (\partial h / \partial x)^2)^{3/2}}$$

and can get dh/dy , etc.

*
→ Capillary Waves.

Recall discussed ocean waves (stable R.T.)



17.

$$\frac{\partial^2 \phi}{\partial t^2} = \frac{\sigma}{\rho} \nabla^2 \frac{\partial \phi}{\partial z} - g \frac{\partial \phi}{\partial z}$$

$$\Rightarrow \boxed{\omega^2 = kg + \frac{\sigma k^3}{\rho}} \quad \rightarrow \text{dispersion relation for capillary waves}$$

note: - capillarity estimate $l \sim \sqrt{\sigma/\rho g}$

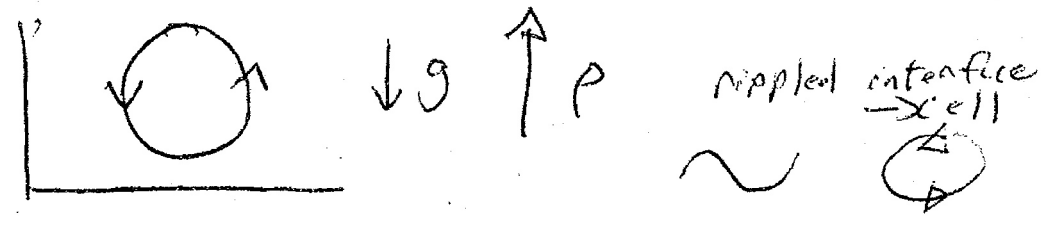
$$\text{d.f.} \Rightarrow k_{\text{cap}}^2 \sim \rho g / \sigma \quad \checkmark$$

- in ocean, capillarity significant at $\leq 5\text{cm}$

- if R.T. unstable, capillarity will cut-off high k instability

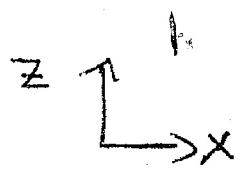
$$\text{i.e.} \quad \omega^2 = \frac{-kg(\rho_2 - \rho_1)}{(\rho_2 + \rho_1)} + \frac{\sigma k^3}{(\rho_2 + \rho_1)}$$

- motion is that of convective cells, vortices



To calculate:

- For 2D cell



$$\frac{\partial \tilde{v}_x}{\partial t} = -\partial_x \left(\frac{p}{\rho_0} \right)$$

$$\frac{\partial \tilde{p}}{\partial t} = -\tilde{v}_z \frac{d\rho_0}{dz}$$

$$\frac{\partial \tilde{v}_z}{\partial t} = -\partial_z \left(\frac{p}{\rho_0} \right) - g \frac{\tilde{\rho}}{\rho_0}$$

Suggests write:

$$\underline{v} = \underline{\nabla} \phi \times \underline{y}$$

$$\Rightarrow \tilde{v}_x = -\partial_z \tilde{\phi}$$

$$\tilde{v}_z = \partial_x \tilde{\phi}$$

$$-\frac{\partial}{\partial t} \partial_z \tilde{\phi} = -\partial_x \left(\frac{p}{\rho_0} \right) \quad (1)$$

$$+\frac{\partial}{\partial t} (\partial_x \tilde{\phi}) = -\partial_z \left(\frac{p}{\rho_0} \right) - g \frac{\tilde{\rho}}{\rho_0} \quad (2)$$

$$\partial_z (1) - \partial_x (2) \Rightarrow$$

$$-\frac{\partial}{\partial t} \nabla^2 \tilde{\phi} = \frac{\partial}{\partial x} \left(g \frac{\tilde{\rho}}{\rho_0} \right)$$

$-\nabla^2 \phi = \omega_y$
 \downarrow
 component
 vorticity

Should be apparent now that:

→ for high k , curvature of crests, etc. becomes sharp

→ before, tacitly took $\rho g \eta \gg \frac{\sigma}{R_L}$
now if $R_L \sim \lambda$ s/t $\lambda^2 \sim \sigma / \rho g$

must retain surface tension in ~~the~~
surface wave dynamics \Rightarrow capillary waves

To include:

$$p = p_0 - \sigma \nabla^2 \eta$$

Then recall: $\frac{\partial \tilde{\phi}}{\partial t} = -\frac{p}{\rho} - g \tilde{\eta}$

$$\frac{\partial \tilde{\eta}}{\partial t} = \frac{\partial \tilde{\phi}}{\partial z}$$

$$\therefore \frac{\partial \tilde{\phi}}{\partial t} = \frac{\sigma}{\rho} \nabla^2 \tilde{\eta} - g \tilde{\eta}$$

$$\frac{\partial \tilde{\eta}}{\partial t} = \frac{\partial \tilde{\phi}}{\partial z}$$

$$\frac{\partial}{\partial t} \nabla^2 \tilde{\phi} = -\frac{\partial}{\partial x} (g \tilde{\rho} / \rho_0)$$

$$\frac{\partial \tilde{\rho}}{\partial t} = -\partial_x \tilde{\phi} \frac{d\rho_0}{dz}$$

$$\frac{\partial^2}{\partial t^2} \nabla^2 \tilde{\phi} = \left(\frac{g}{\rho_0} \frac{d\rho_0}{dz} \right) \frac{\partial^2 \tilde{\phi}}{\partial x^2}$$

$$\Rightarrow +\omega^2 k^2 = \left(\frac{g}{\rho_0} \frac{d\rho_0}{dz} \right) (-k_x^2)$$

$$\omega^2 = -\frac{k_x^2}{k^2} \left(\frac{g}{\rho_0} \frac{d\rho_0}{dz} \right)$$

$\hookrightarrow > 0$, as $d\rho_0/dz > 0$

$$\therefore \gamma = \sqrt{\frac{k_x^2}{k^2} \left(\frac{g}{L_p} \right)^{1/2}} \rightarrow \text{R.T. Convective cell growth-rate}$$

Then:

→ structure similar to Rayleigh - Bénard convection

ie. $\frac{\partial}{\partial t}$ vorticity = torque / buoyancy (RB) / gravitational force (RT)

$\rightarrow k_x \rightarrow \infty \Rightarrow \gamma \rightarrow \frac{g}{L_p}$

Thus, to incorporate finite interface thickness in RT growth formula

$$\begin{aligned} \gamma &\sim \sqrt{gAk} & kL_p < 1 \\ &\sim \sqrt{g/L_p} & kL_p > 1 \end{aligned}$$

$$\Rightarrow \gamma = \left(gAk / (1 + kL) \right)^{1/2}$$

↓ ↓
scale factor, interface.

∴ $kL > 1 \Rightarrow$ growth rate saturates!

→ For stable stratification $dp_0/dz < 0$

$$\omega^2 = \frac{k_x^2}{k^2} \frac{g}{\rho_0} \left| \frac{d\rho_0}{dz} \right| \equiv \frac{k_x^2}{k^2} N^2 \rightarrow \text{BV freq}$$

→ dispersion relation for oceanic internal wave

→ finite density gradient analogue of (interface) surface wave

→ interesting to note effects of viscosity
particle diffusivity

viscosity $\frac{\partial}{\partial t} \nabla^2 \phi \rightarrow \left(\frac{\partial}{\partial t} - \nu \nabla^2 \right) \nabla^2 \phi$

diffusivity $\frac{\partial}{\partial t} \rho \rightarrow \left(\frac{\partial}{\partial t} - D \nabla^2 \right) \rho$

\Rightarrow

$$(\omega + i\nu k^2)(\omega + iDk^2) = -\frac{k_x^2}{k^2} \frac{g}{\rho_0} \frac{d\rho_0}{dz}$$

i.e. $\left\{ \begin{array}{l} \nu k^2 \gg \omega \\ D \rightarrow \infty \end{array} \right.$ (viscous fluid)

$$(i\nu k^2)(i\nu) = -\frac{k_x^2}{k^2} \frac{g}{\rho_0} \frac{d\rho_0}{dz}$$

$$\nu = \frac{k_x^2}{k^2} \left(\frac{g}{\rho_0} \frac{d\rho_0}{dz} \right) / \nu k^2$$

$\rightarrow \nu \sim 1/\nu k^2$

\rightarrow strong viscosity reduces growth rate
but instability persists
(i.e. molasses + air!)

i.e.

\Rightarrow

$$\gamma^{\bullet} = \left(\frac{k_x^2}{k^2} \frac{g}{\rho_0} \frac{d\rho_0}{dz} \right)^{1/2} - \nu k^2$$

i.e. viscosity and diffusivity can stabilize
RT instability
→ defines critical D/δ

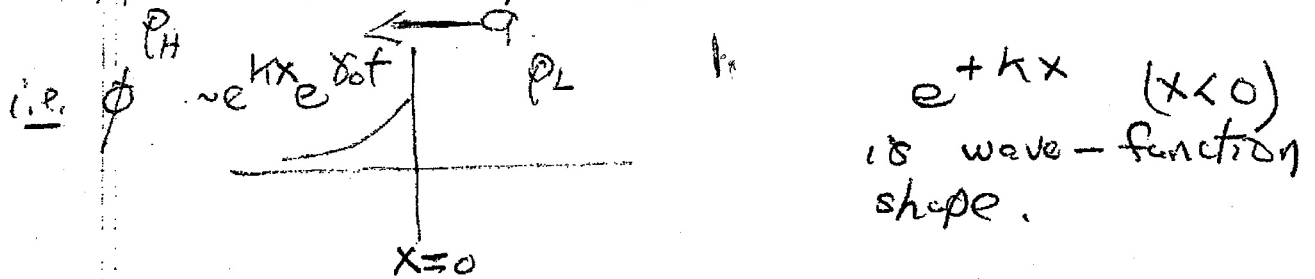
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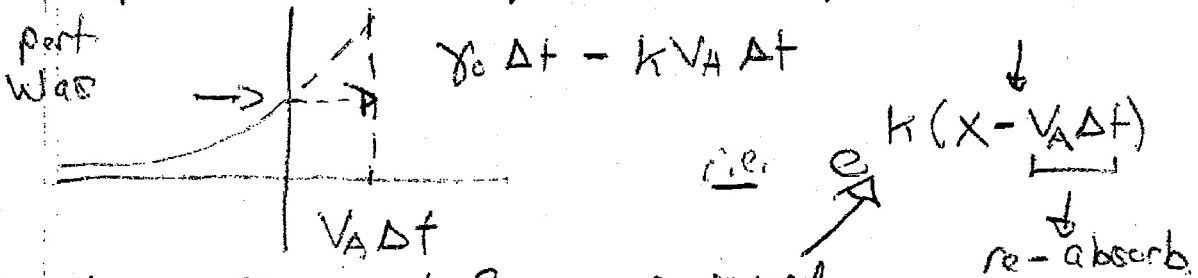
(i) Ablation (Ablation critical element of environment imploded \rightarrow ablation driven pocket)

\rightarrow physical concept is that due to heating, material streams away from interface, \therefore can't participate in RT instability

\rightarrow heuristic interpretation:



with ablation, hot matter "blown off" \Rightarrow interface displaced inward



blow-off \Rightarrow interface moves inward

i.e. $\phi \sim e^{k(x - V_A \Delta t)} e^{\gamma_0 \Delta t}$
 $\sim e^{kx} e^{(\gamma_0 - k V_A) \Delta t}$

$V_{abl} \equiv \frac{\dot{M}}{\rho A}$

\therefore ablative blow-off yields stabilizing effect

$\gamma = \gamma_0 - k V_A$; $\gamma_0 = \sqrt{k g}$

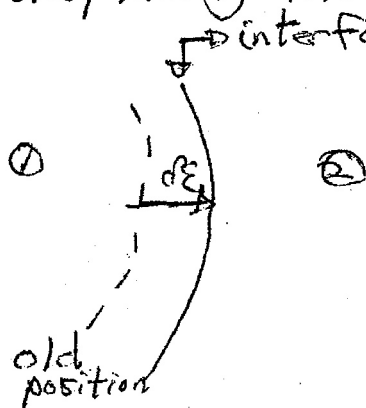
Insert ~~III~~ Surface Tension

→ Consider two liquids separated by a thin (i.e. few molecules) interface



Now, consider displacing the interface toward 2 by δx

i.e.



(see 1)

∴ can determine change in free energy (i.e. thermodynamic sense) via:

$$dF = \underbrace{dF_1 + dF_2}_{\text{bulk phases}} + dF_{\text{interface}}$$

↳ treat as separate constituents

Recall: $dF = -SdT - pdV$

(i.e. $F = E - ST$)

$$dF_{1,2} = (-SdT - pdV)_{1,2}$$

(i.e. the usual)

→ no simple, rigorous analytical theory exists!

Aside: For ICF, can combine finite interface thickness and ablative stabilization to control RT growth (A=1)

i.e. simple RT $\gamma = \sqrt{kg}$

finite interface $\rightarrow \gamma = \left(\frac{kg}{1+kL_0} \right)^{1/2}$

ablation $\rightarrow \gamma = \left(\frac{kg}{1+kL_0} \right)^{1/2} - kVA$

By $\left. \begin{array}{l} - \text{target design } - L_0 \\ \text{(structure)} \\ - \text{materials, etc } - VA \\ \text{(loading)} \end{array} \right\} \text{ can minimize implosion pert. growth}$

(V₀) Spherical Geometry - Postpone till later

Credely:
$$\begin{cases} \omega \sim \sigma/u \\ Lu \sim \# \sqrt{g\lambda} \end{cases}$$

N.B. : { Can solve 3 bubble Layer model (numerically) to determine # in merger rule.